



**Shell Catalysts & Technologies**

## **High-performance tail-gas treating**

**Hans Wijnbelt**

Tail Gas Application  
Specialist

**Karl Krueger**

Senior Research  
Scientist

**Michael Huffmaster**

Consultant



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# Speakers



**Hans Wijnbelt**  
**Tail Gas Application Specialist**  
Shell Catalysts & Technologies



**Karl Krueger**  
**Senior Research Scientist**  
Shell Catalysts & Technologies



**Michael Huffmaster**  
**Consultant**

# Outline

## WHY?

- The drivers for Shell developing SCOT technology and tail-gas treating catalysts
- Environmental Duty and Technology Advancements

## HOW?

- Our approach to catalyst development projects, with a specific focus on tail-gas treating catalysts
- The processes, technology, analytics and equipment we use

## WHAT?

- The catalyst products we have developed
- Key applications

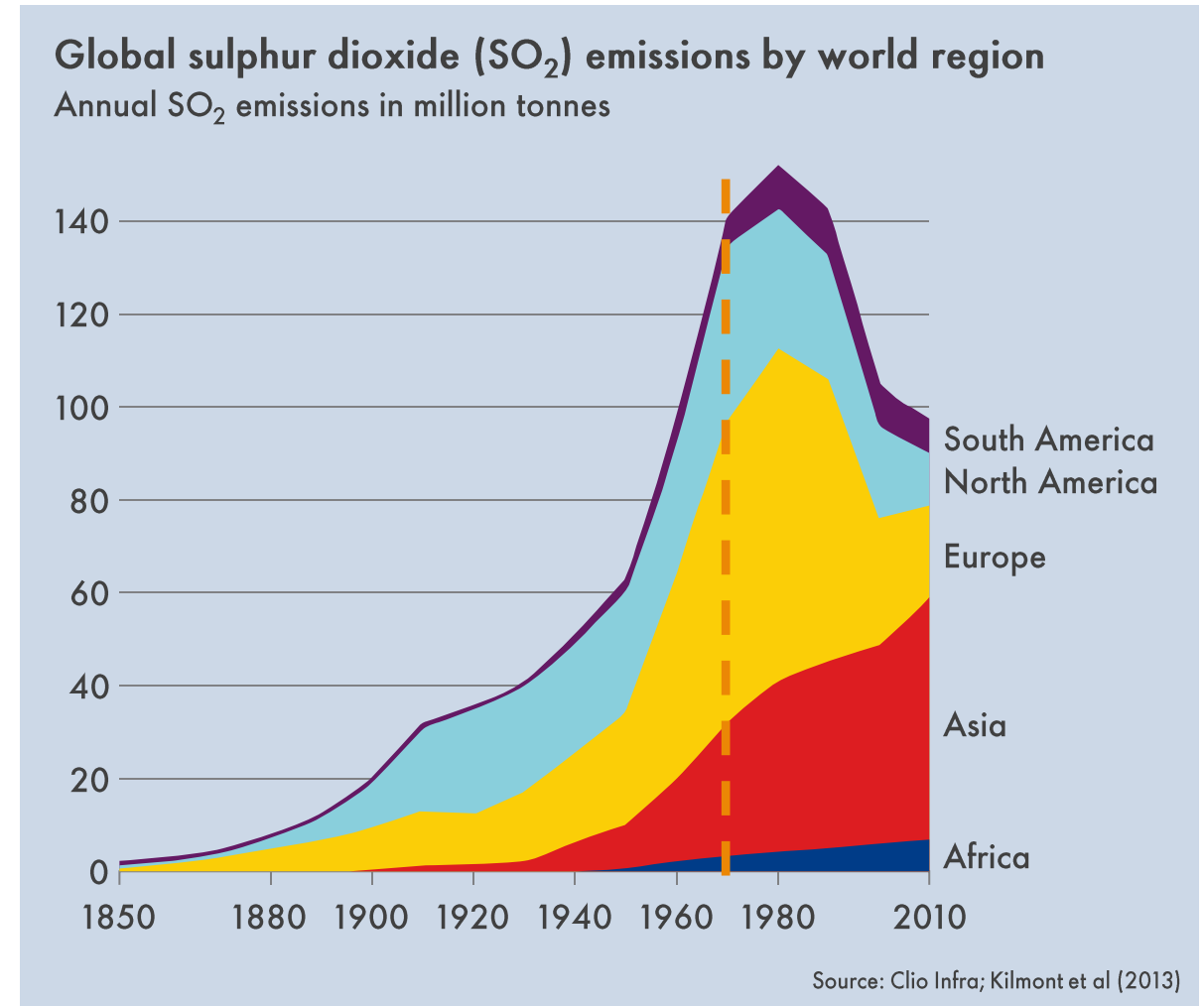
## 934

- A new state-of-the-art SCOT tail-gas catalyst that sets superior performance standards in low-temperature operation
- Opportunities and the potential value to you

# Shell Claus Offgas Treating (SCOT) process history

- Global initiatives in 1970s legislate reduction in sulphur emissions
- SCOT is the most widely applied TGU technology and catalyst
- 1970 – Shell awarded patent for using hydrotreating with amine for tail-gas treating
- 1972 – First application (Japan)
- 1975 – First US application (Norco)

50 years working on reducing SO<sub>2</sub>



# Why SCOT

## The industry standard

The most commercially proven tail-gas clean-up process when tail-gas recoveries in the 99.9% range are required



**260+ units**  
worldwide



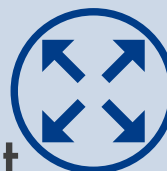
**10ppmv H<sub>2</sub>S** specification in the SCOT vent gas can be achieved with Low-Sulphur SCOT

Application in **E&P**  
and **refining**



**3 t/d to 4000 t/d**

sulphur capacities of upstream Claus unit

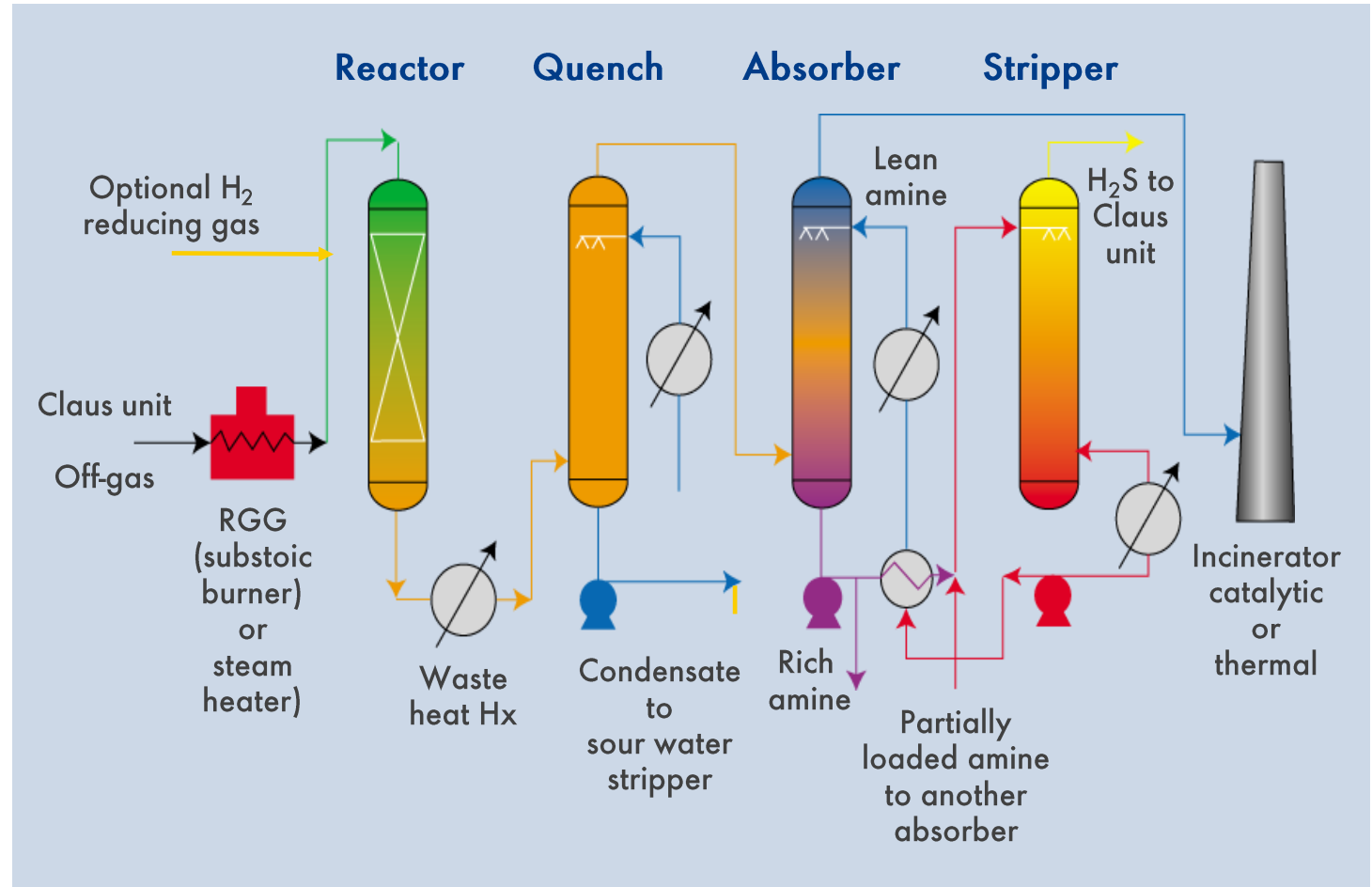


Ultra-high sulphur recovery efficiency:  
**99.7+%** (SCOT)  
**99.95%** (SCOT ULTRA)



# SCOT process: Sulphur species in Claus tail gas $\rightarrow$ $\text{H}_2\text{S}$ $\rightarrow$ Claus

- High activity, low DP catalyst cobalt/molybdenum on alumina
- Reducing gas generator (RGG) burner for application w/o  $\text{H}_2$
- Standalone amine system
- High reliability – 99%+ availability
- Turndown
- Configurations
  - Integrated/cascade
  - Low-Temperature SCOT
  - Low-Sulphur SCOT
  - SCOT ULTRA



# SCOT process innovation

## Continuing improvement across 50 years

### Conventional

- RGG + Reactor + Quench + standalone amine
- Booster blower when required

### Quench and amine

- Selectivity – CO<sub>2</sub> slip – DIPA, MDEA, Specialty solvent
- Pressure drop – trays to packing
- Booster blower deleted

### Integrated and cascade options

### Low Sulphur performance

- Super stripper regeneration
- Acid aided regeneration
- Specialty sterically hindered solvent

### Low temperature capability

- Reactor inlet as low as 200°C
- Higher activity catalyst
- Steam preheat and lower CAPEX
- OPEX reduction – energy

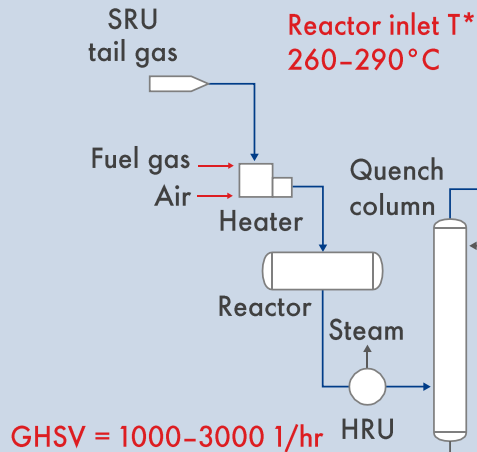


**Design expertise and catalyst development  
combined with operational experience**

# Sulphur recovery system – Low-temperature tail-gas unit

## Conventional configuration

Inlet pressure  
0.15–0.30 bar

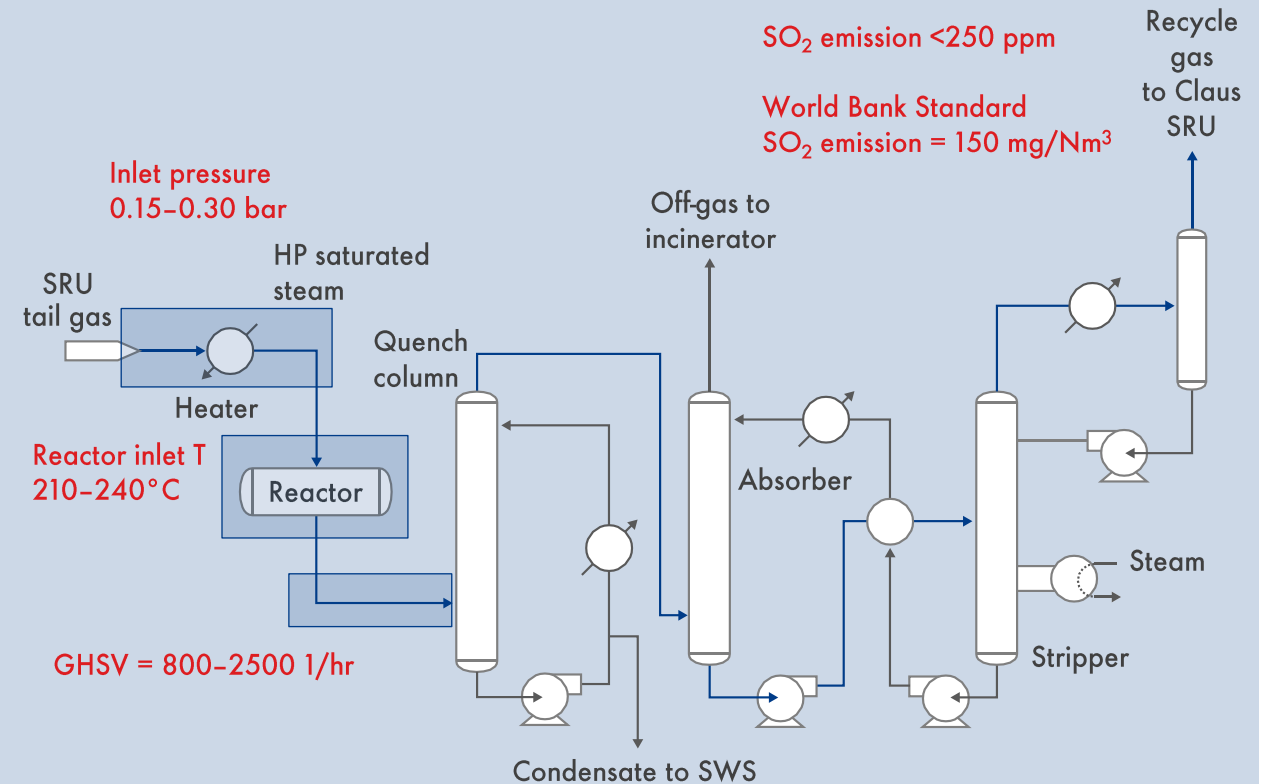


\*In-line heater may operate either conventional or low-temperature mode

## Benefits of low-temperature technology:

- Condensing steam preheat vs RGG burner
- HRU deleted
- Reduced CAPEX
- Lower temperature  
Reduced heat input
- Lower OPEX
- Improved operability
- Needed:  
Higher activity catalyst

## Low-temperature trend in tail-gas technology



Higher activity catalyst is required

# Low-temperature effects

## Benefits

- Indirect preheat option (condensing steam)
- Burner and controls are eliminated – avoids major causes for catalyst damage
- 10–15% less CAPEX
- Lower fuel rate and less instrument and electrical maintenance means reduced OPEX
- Smaller carbon footprint

## Challenges

- Diminished catalytic activity at low temperature; requires more catalyst or higher activity catalyst
- Impact of undesirable reactions, COS survival and mercaptan formation slip past the amine system and on to incinerator
- Requires a bit higher hydrogen concentration

# SCOT catalyst development

Reactors utilise catalysts with cobalt and molybdenum sulfides on alumina support, active sites for hydrolysis, hydrogenation and water gas shift (WGS)

- First generation: Specifically developed from initial re-purposed hydrotreating catalysts
  - Second generation: developed high activity, high porosity, long life
    - Third generation: High activity contemporary low-temperature catalyst
  - **934 is newest, most active, more effective low-temperature activation**

|                            | RIT, °C | RIT, °F | WABT, °C | WABT, °F | αGHSV (1/hr) |
|----------------------------|---------|---------|----------|----------|--------------|
| First generation (534)     | 280     | 540     | 300–330  | 570–630  | 1000–2000    |
| Second generation (234)    | 240     | 465     | 250–300  | 480–570  | 2000–2500    |
| Third generation (LT-834)  | 220     | 430     | 230–250  | 445–480  | 1500–2000    |
| Latest generation (LT-934) | 200     | 392     | 210–230  | 410–445  | 1500 - 2000  |

Catalyst products (234 , 534, 834 or 934) arise from a continuing commitment by Shell for environmental improvement and a progression of development over 50 years for enhancing performance and activity

## Key technology differentiators

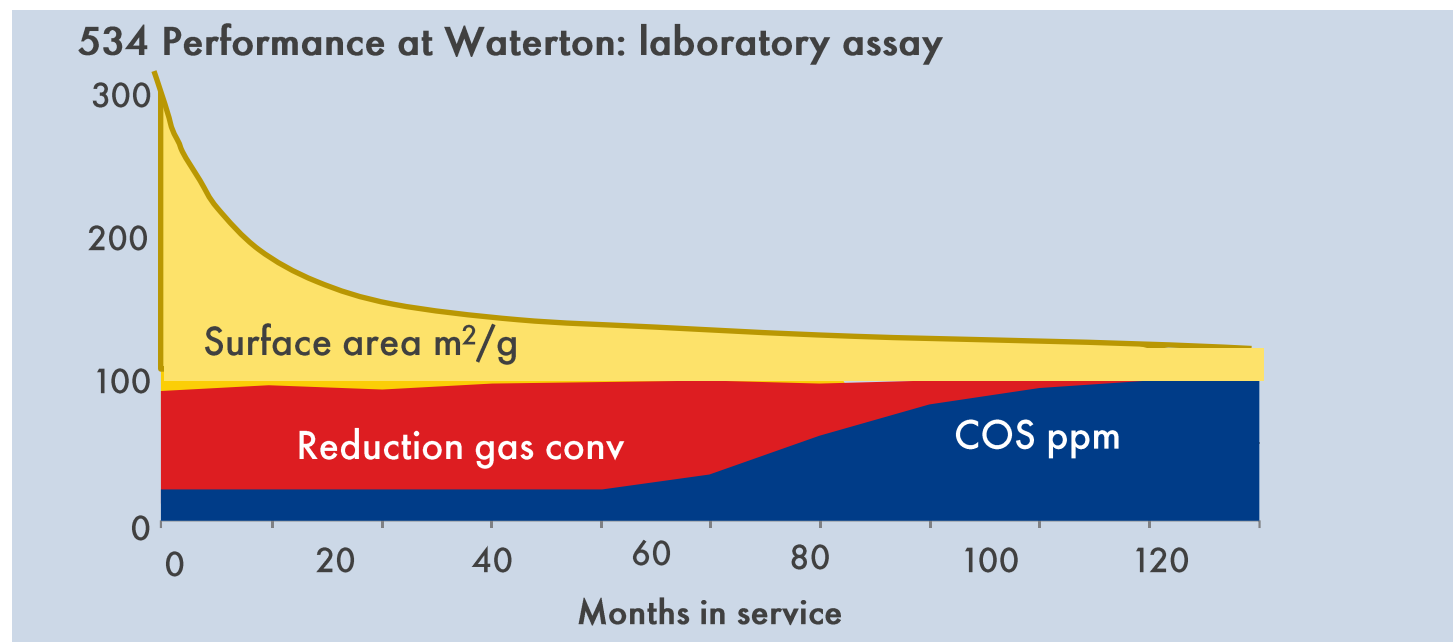
- Advanced low temperature SCOT catalyst means reactor inlet can be as low as 200°C
- Cascaded SCOT unit offering reduces the overall solvent requirement
- SCOT process demonstrates robust operability  
good overall sulphur recovery even during substantial upsets in the Claus  
downtime experience is ~0.5% for SCOT units
- SRU can operate on a continuous basis at 10–100% of design capacity
- SCOT can start up with less than 10% of design feed

**Catalyst innovations and process technology advancements have enhanced operability and provided significant savings in CAPEX and OPEX**

# SCOT process and operational support

## SCOT catalyst life

- Aging factors include hydrothermal, carbon, sulfation, whacking
- Activity follows surface area, declining to 50% from SOR to EOR
- 4–6 years is typical service life
- 12+ years has been achieved
- Catalyst activity is stronger at higher temperature
- 934 is a more active catalyst, performing at lower temperature, with operating allowance to raise temperature and extend run



## What we provide

- **SCOT catalyst:** Selection assistance for best practice in catalyst life
- **Assessment:** Evaluate catalyst activity from plant performance data, Project remaining catalyst life
- **SCOT process:** Providing operations guidelines, training and advice

# Drivers for tail-gas catalyst improvement



Shell responding to demand  
for higher activity catalyst

Industry focus  
on further  
reducing  
OPEX (fuel)  
and enhancing  
operability

World Bank standards  
tighter emission requirements

Requirement to operate  
at lower temperatures



Our new catalyst should offer lower energy consumption, full activation at low temperature, higher activity at low temperature, increased catalyst lifecycle and improved conversion and lower emission of  $\text{SO}_2$ ,  $\text{CO}$  and  $\text{CO}_2$

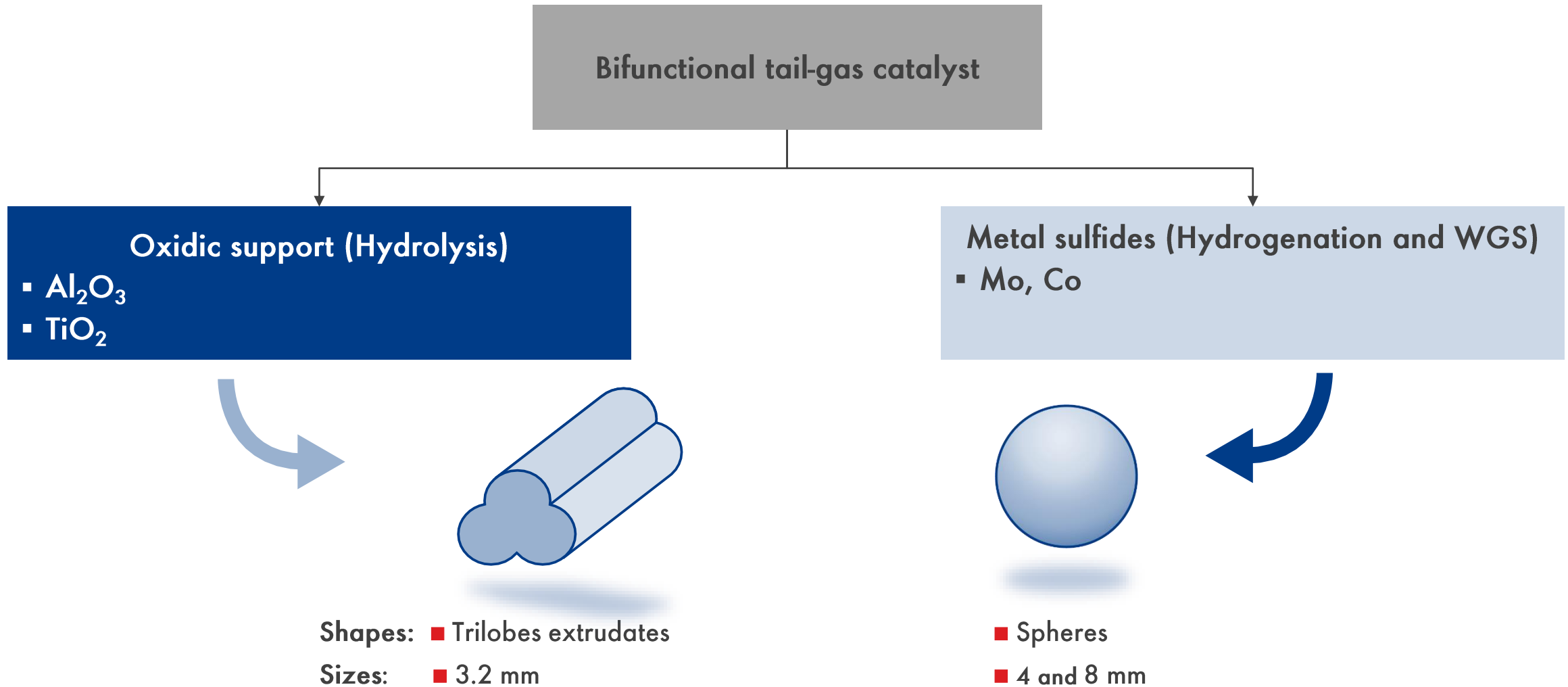
# The catalyst is the key

Low-temperature operation is only possible with high-activity catalysts

Traditional catalysts simply don't perform reactions fast enough to be operated at low temperature

|                                     |   |                                             |   |                             |
|-------------------------------------|---|---------------------------------------------|---|-----------------------------|
| $\text{SO}_2 + 3\text{H}_2$         | → | $\text{H}_2\text{S} + 2\text{H}_2\text{O}$  | → | $\text{SO}_2$ hydrogenation |
| $\text{SO}_2 + 2\text{H}_2$         | → | $\text{S} + 2\text{H}_2\text{O}$            | → | $\text{SO}_2$ hydrogenation |
| $\text{S} + \text{H}_2$             | → | $\text{H}_2\text{S}$                        | → | $\text{S}$ hydrogenation    |
| $\text{COS} + \text{H}_2\text{O}$   | → | $\text{CO}_2 + \text{H}_2\text{S}$          | → | $\text{COS}$ hydrolysis     |
| $\text{CS}_2 + 3\text{H}_2$         | → | $\text{CH}_3\text{SH} + \text{H}_2\text{S}$ | → | $\text{CS}_2$ hydrogenation |
| $\text{CS}_2 + \text{H}_2\text{O}$  | → | $\text{COS} + \text{H}_2\text{S}$           | → | $\text{CS}_2$ hydrolysis    |
| $\text{CH}_3\text{SH} + \text{H}_2$ | → | $\text{CH}_4 + \text{H}_2\text{S}$          | → | Mercaptan hydrogenation     |
| $\text{CO} + \text{H}_2\text{O}$    | → | $\text{CO}_2 + \text{H}_2$                  | → | $\text{CO}$ WGS             |

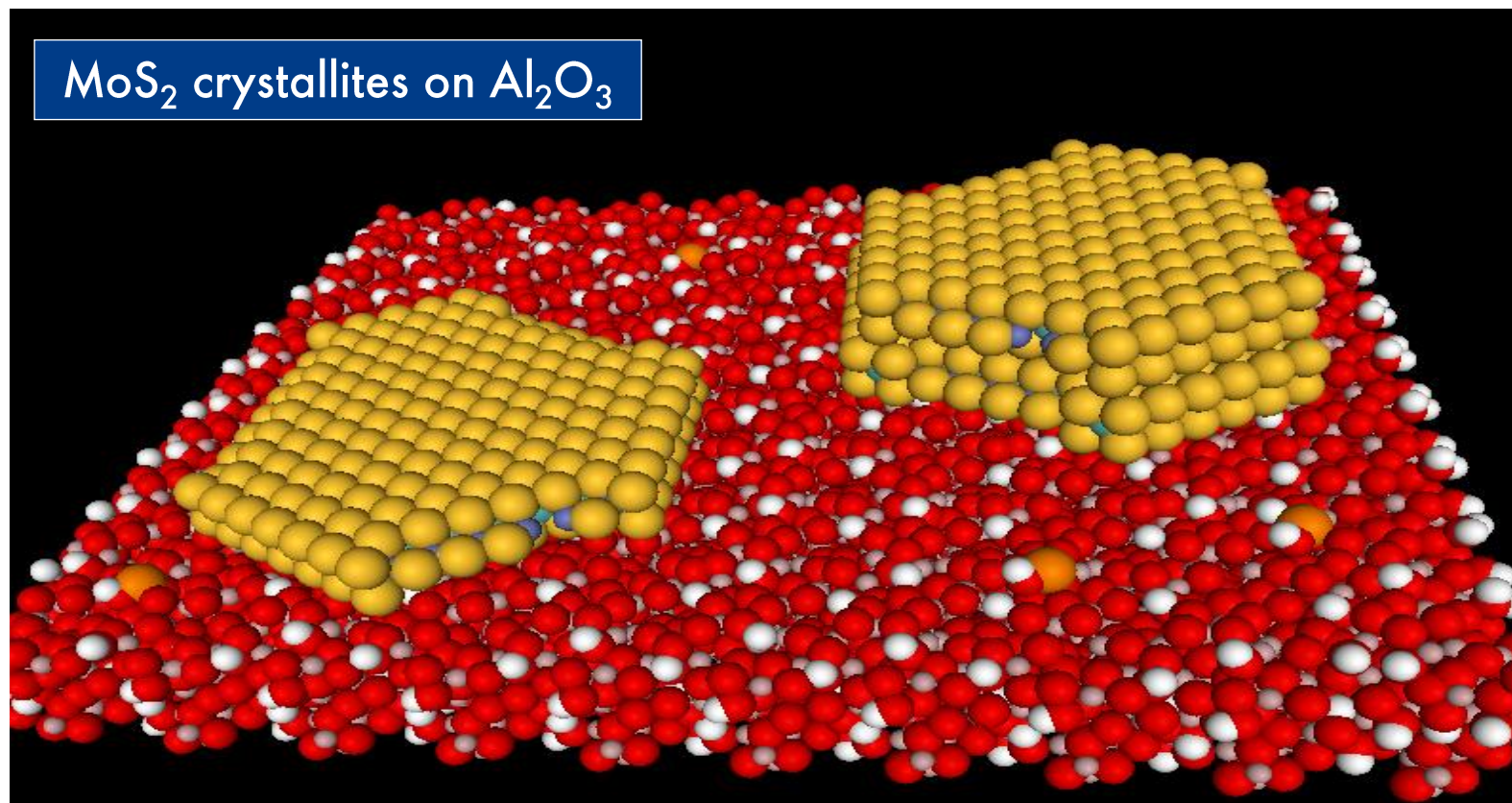
# Composition of commercial tail-gas treating catalysts



# Tail-gas catalyst active sites

**Co-Mo-S phase: Hydrogenation and WGS occur on these slab structures**

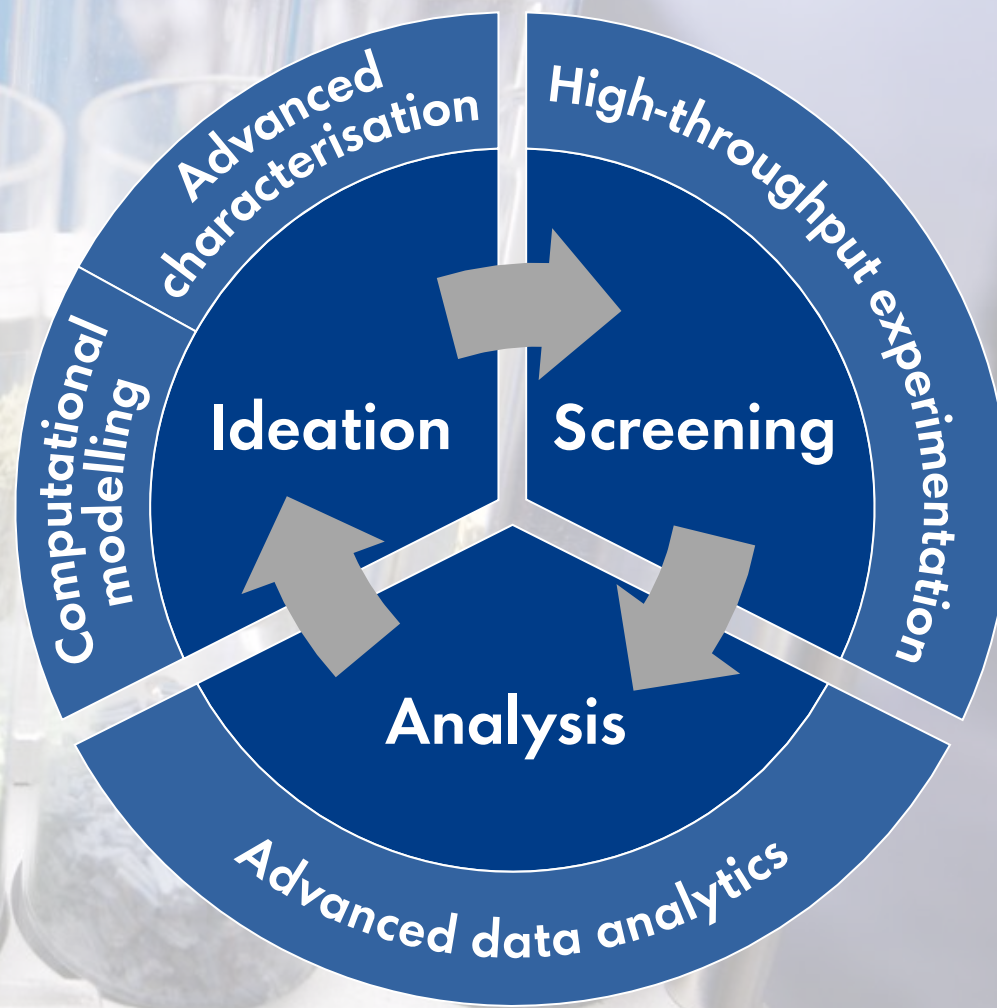
**Alumina: Hydrolysis occurs on the highly porous support (alumina phases affect activity)**



|   |         |
|---|---------|
| ■ | S       |
| ■ | Co      |
| ■ | O       |
| ■ | O       |
| ■ | Al      |
| ■ | Dopants |

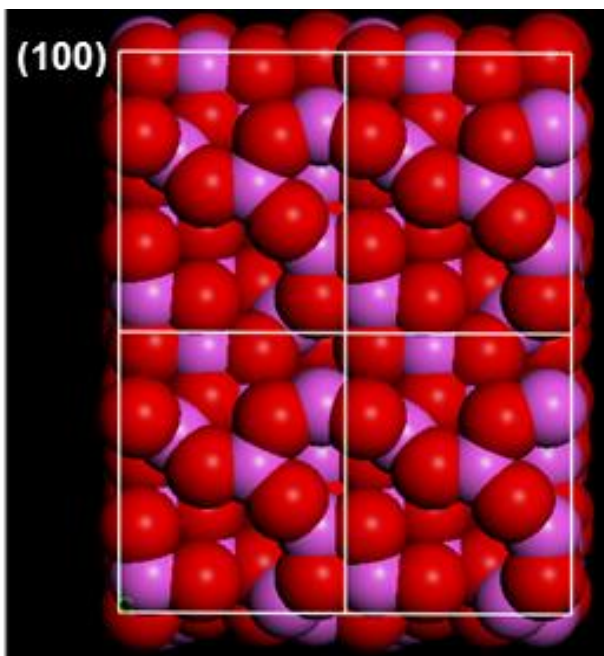
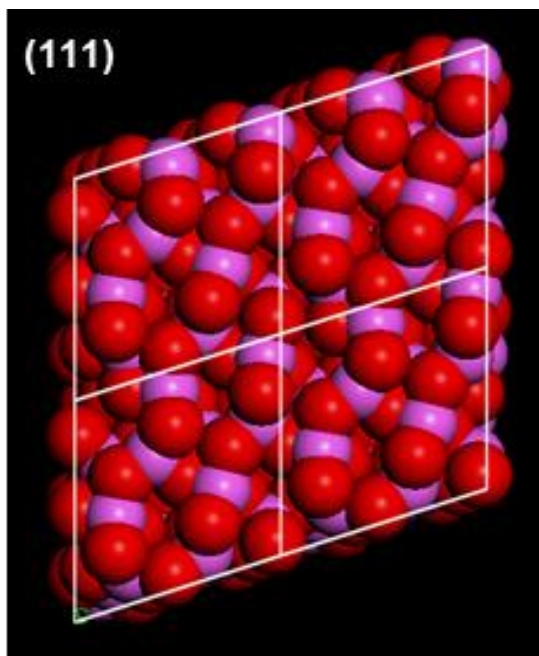
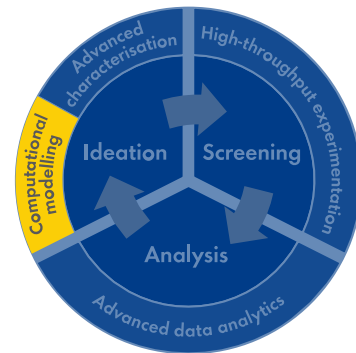
# Shell Catalysts & Technologies' catalyst development process

- Parallel workflow: Ideation, screening and analysis occur simultaneously
- Eliminates barriers to invention
- Enabled by major investments in:
  - Computational modelling
  - Advanced characterisation
  - High-throughput experimentation
  - Advanced data analytics
- Recognises the importance of each part of the process



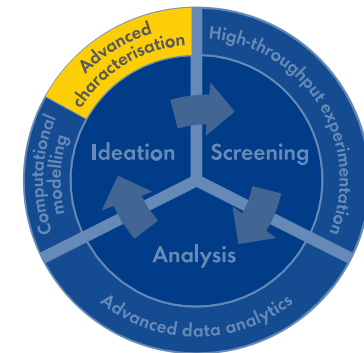
# Computational modelling

- Elucidates key descriptors of catalyst activity
- Allows the optimisation of these descriptors as well
- Synthetic strategies are guided by these learnings
- Fewer physical experiments needed to obtain higher activity

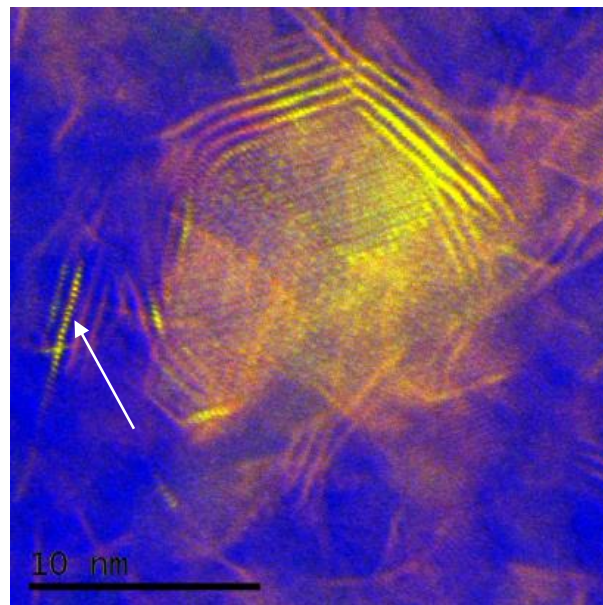
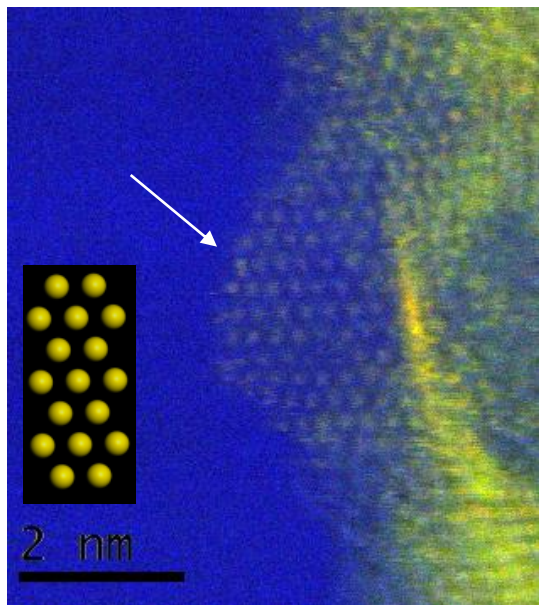


Density function theory calculation to determine optimal aluminum and oxygen placement in the catalyst support

# Advanced characterisation

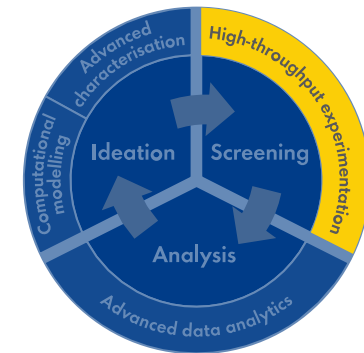


- Provides a fundamental understanding of the structure/function relationship
- These learnings allow the custom tailoring of catalysts for high performance
  - E.g. Incorporating direct and indirect desulphurisation active sites into individual  $\text{MoS}_2$  slabs



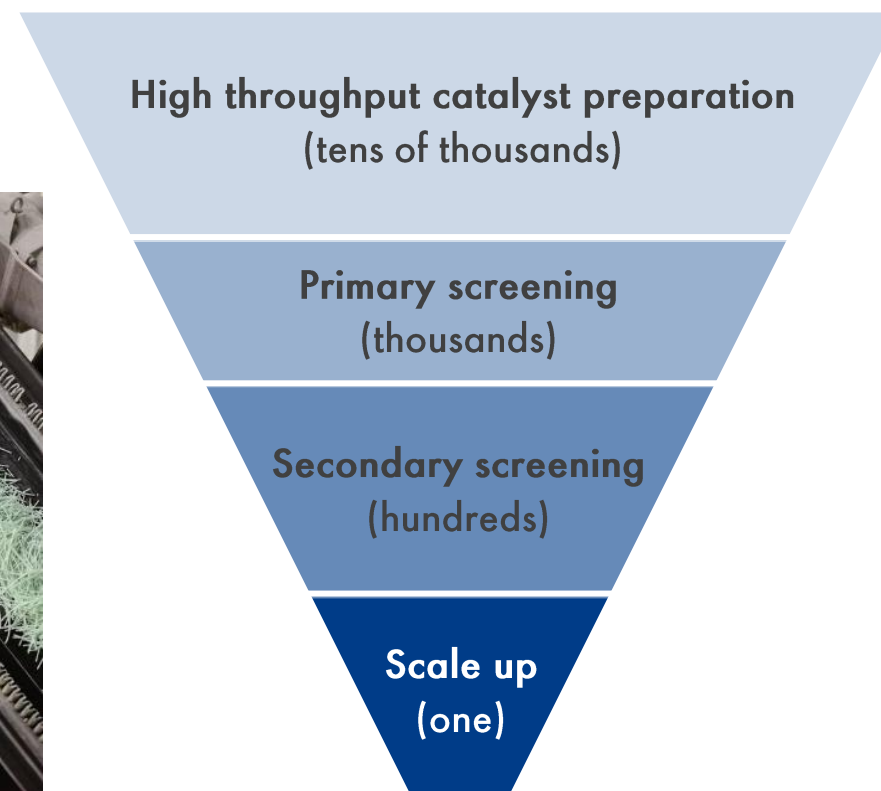
Aberration-corrected transmission electron microscopy allows us to see the active sites of real catalysts operating on customer feedstocks

# High-throughput experimentation



- Screen ideas as quickly and accurately as possible
- Funnel systematically sieves through formulations
  - High-throughput catalyst preparation
  - Fit-for-purpose catalyst testing
- Allows ideas to be screened that would normally have been ignored

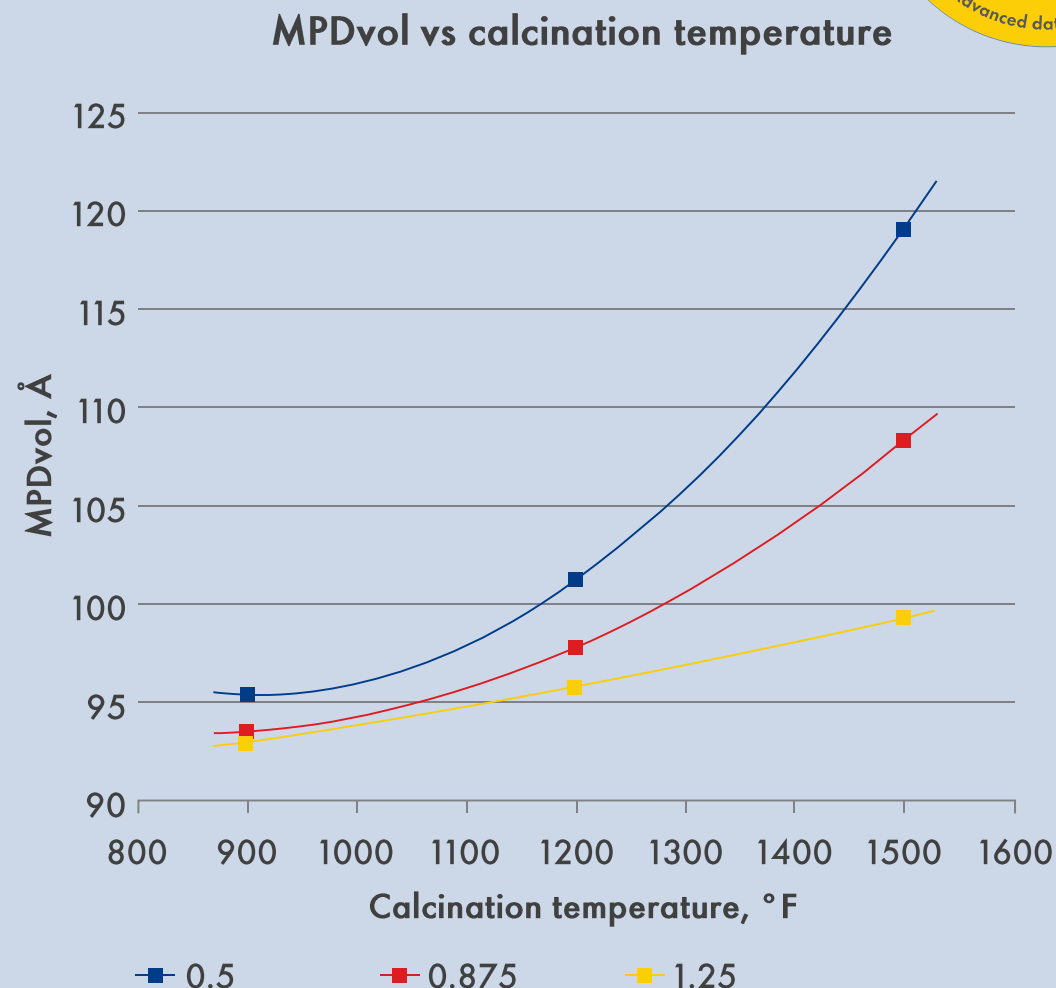
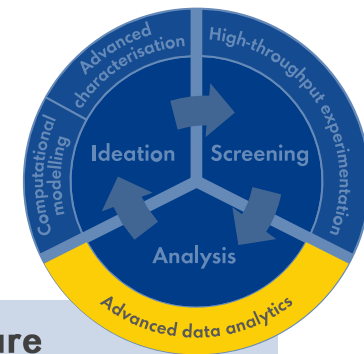
## High throughput funnel



# Advanced data analytics

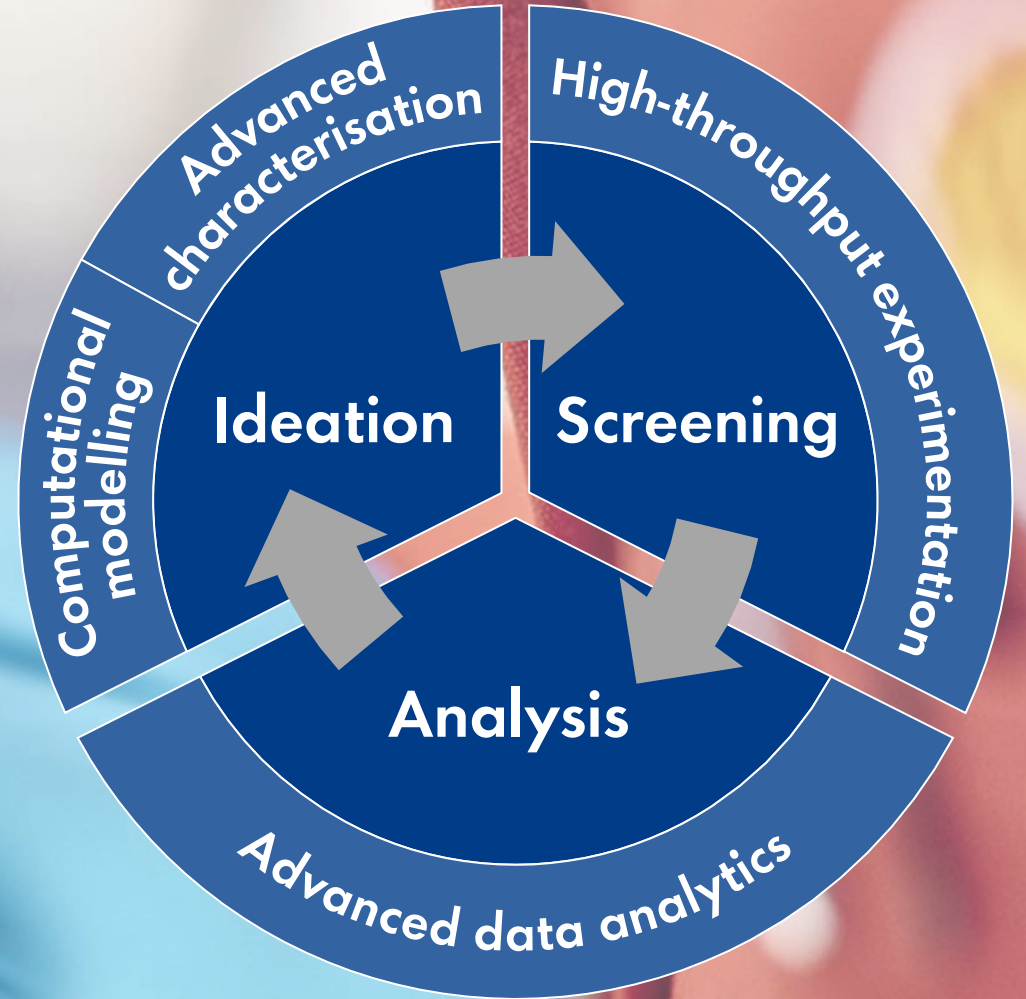
- A natural and essential partner to high-throughput experimentation
- A custom designed software suite encompasses the entire workflow from experimental design to data processing
- Allows the vast data gathered from high-throughput experimentation to be managed and processed
- Statistical models are developed using the entire database rather than incomplete subsets

Statistical analysis finds correlations between variables



# Our catalyst development process helps us to...

- ...generate ideas with a high probability of success
- ...screen those ideas as quickly as possible
- ...extract as many learnings as possible from that data



# Our tail-gas treating catalyst portfolio



**834**

- Operating temperature: as low as 220°C – 428°F
- High activity
- Excellent pressure drop performance



**234**

- Typical operating temperature: 240°C – 465°F
- Balances fill cost and activity
- Excellent pressure drop performance



**534**

- Typical operating temperature: 280°C – 540°F
- Suitable for in-line burner configurations
- Industry-leading pressure drop performance

# Our tail-gas treating catalyst portfolio **just got better**



**934**

- Operating temperature: As low as 200°C – 392°F
- Highest activity, hydrogenation and hydrolysis performance
- Excellent pressure drop performance



**834**

- Operating temperature: as low as 220°C – 428°F
- High activity
- Excellent pressure drop performance



**234**

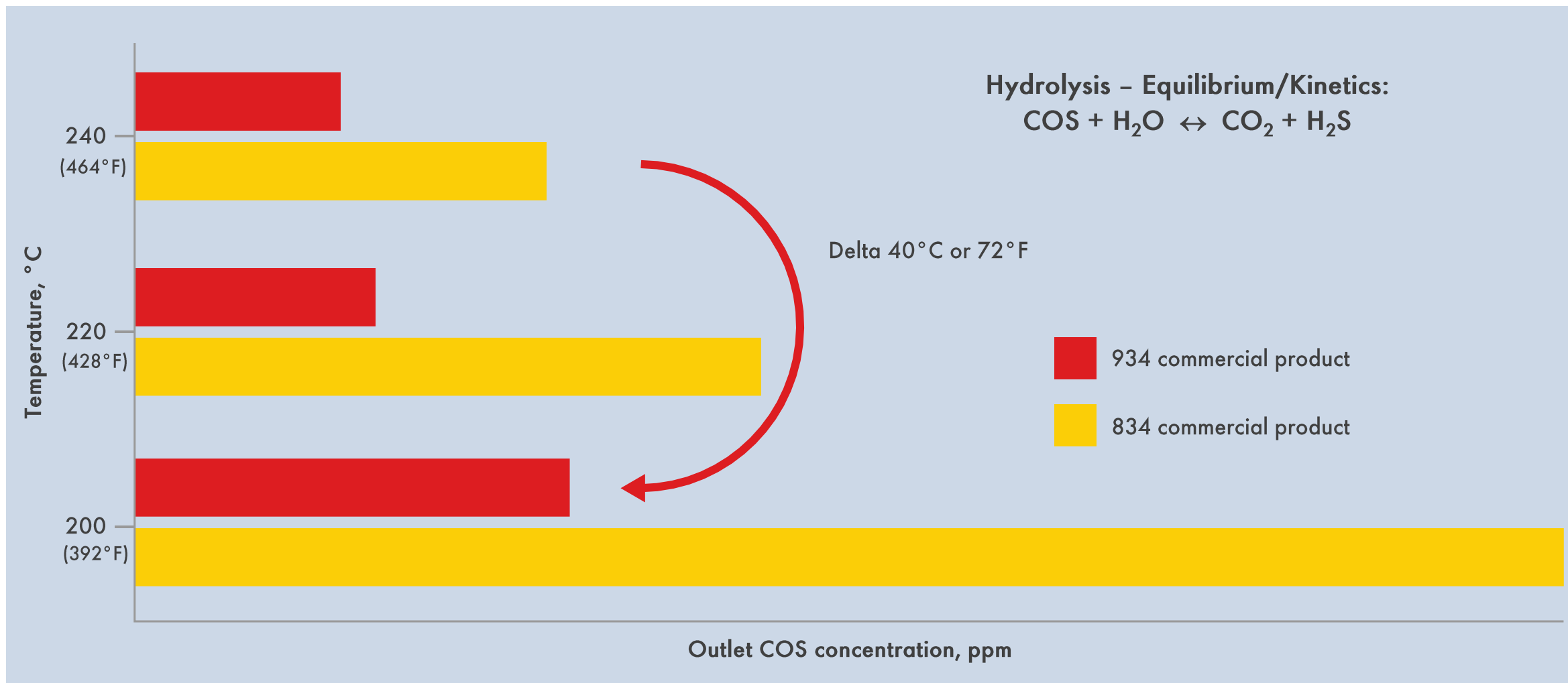
- Typical operating temperature: 240°C – 465°F
- Balances fill cost and activity
- Excellent pressure drop performance



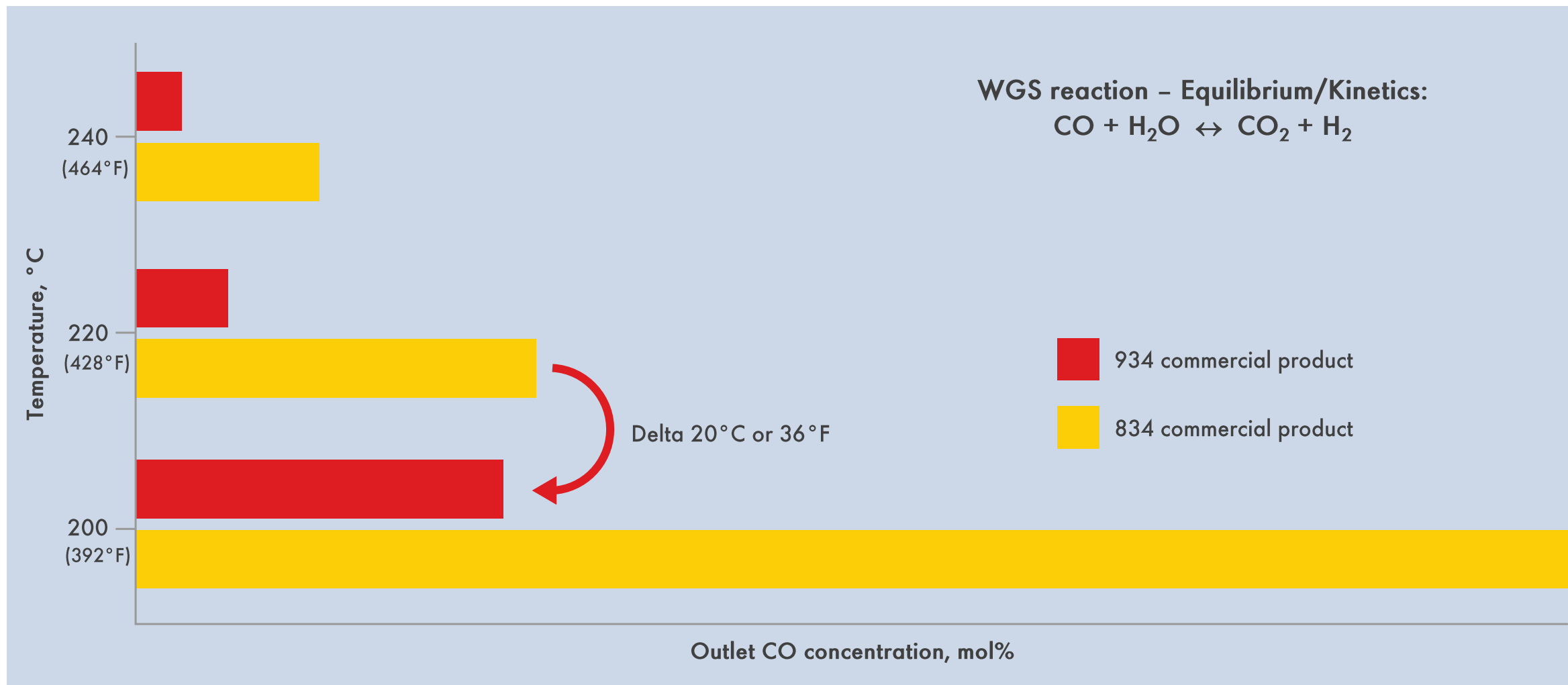
**534**

- Typical operating temperature: 280°C – 540°F
- Suitable for in-line burner configurations
- Industry-leading pressure drop performance

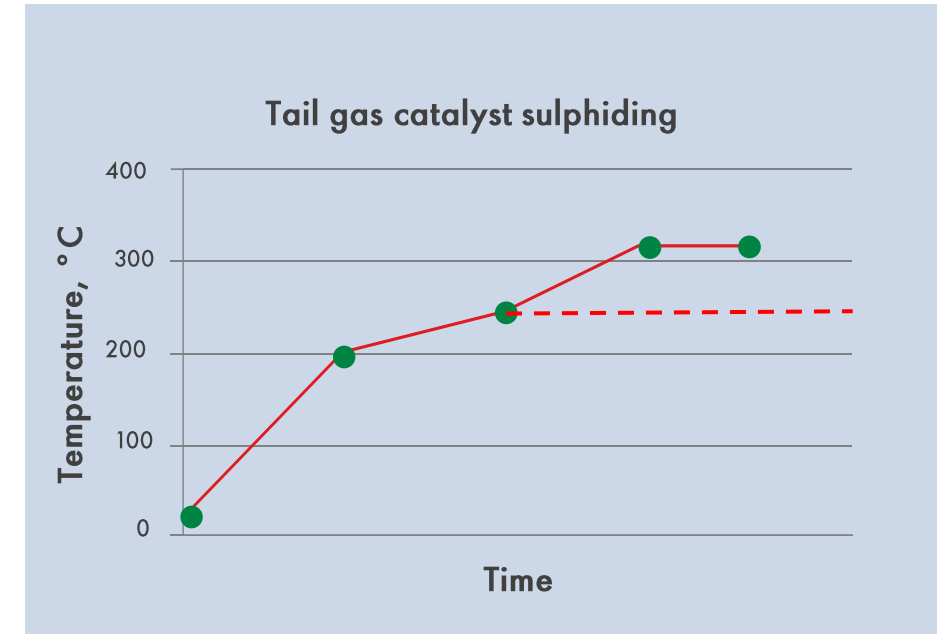
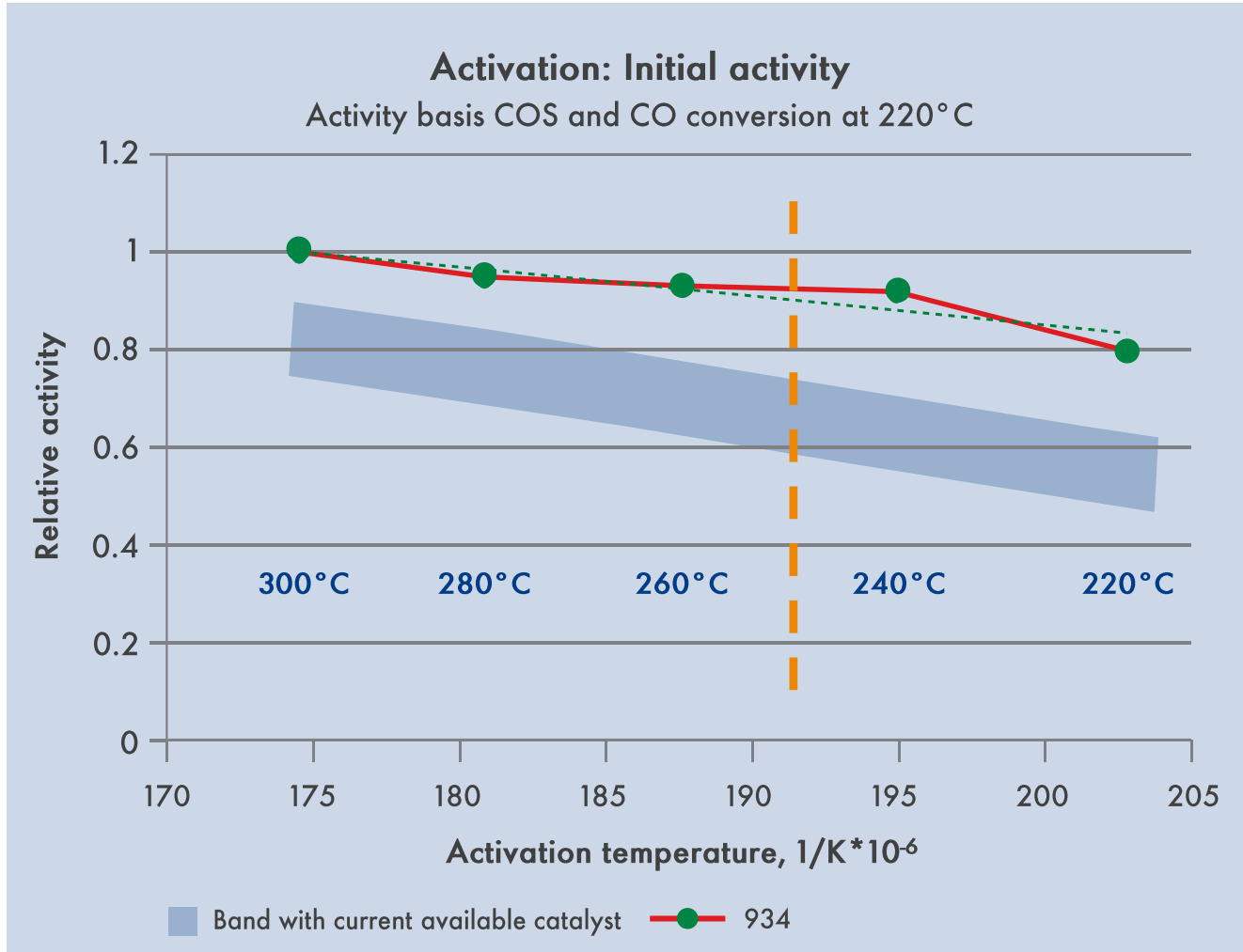
## 934 higher activity and higher selectivity for COS conversion



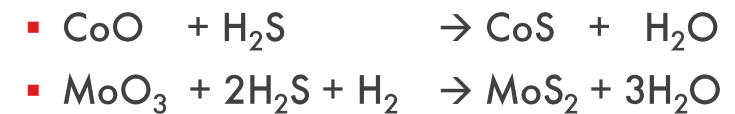
## 934 higher activity and higher selectivity for CO conversion



# 934 benefits from improved catalyst activation



## ■ Catalyst Sulfiding



## 934 is likely to be a strong candidate for your unit if you...

...are able to operate at lower temperatures (Energy reduction)

...experience SO<sub>2</sub> emission issues from COS or CS<sub>2</sub> (Emission constraints)

...have tight limits on CO emissions (Emission constraints)

...are designing a new unit that operates at low temperature using steam or electrical heating (Greenfield)

...have an older type unit and the current burner can undergo a basic upgrade for operation at low temperature (Brownfield)



## 934 case study



### Customer drivers

- Energy reduction target: >10% and reduce CO<sub>2</sub>
- OPEX cost reduction target: 15%
- COS level EOR max 25 ppm
- Catalyst life cycle of 4 years



### Results

- System can handle a 210°C RIT using 934
- Even at lower temperature the expected COS value at EOR will be met
- Lowering temperature from 240°C to 210°C reduces Energy consumption



### Impact

- \$221k/y fuel gas savings
- Reduced SO<sub>x</sub> emissions by lowering COS
- Reduced CO<sub>2</sub> emissions
- Reducing energy use



- Energy savings for four units \$884k/y
- Energy and OPEX saving of 20.5%
- COS at EOR will be lower than 15 ppm



# The takeaways

## WHY?

To help refiners respond to ever-tighter emissions mandates, and other business drivers, we have been developing innovative tail-gas treating catalysts and processes for over 50 years because the environment matters

## HOW?

Our catalyst development process is key: It helps us to generate ideas with a high probability of success, screen those ideas as quickly as possible, and extract as many learnings as possible from that data

## WHAT?

Our portfolio of 234, 534 and 834 is designed to help meet a wide range of refiners' performance objectives, and we just launched **934**, which offers a step change in activity

## 934

- Operating temperatures as low as 200°C are possible; can help extend cycle life
- Potential energy reductions of 20% (case specific)
- higher hydrolysis performance, higher WGS, low pressure drop

